

## DPP No. 32 &amp; 50

## SOLUTION

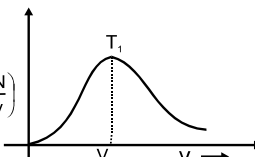
# Hints & Solutions

## DPP No. # 32

6. 
$$\text{N}_2 + 3\text{H}_2 \longrightarrow 2\text{NH}_3$$
- Initially a atm                      b atm  
 Finally a - x                      b - 3x                      2x
- $\therefore a + b = 1$  and  $a + b - 2x = 0.75$   
 $\therefore P_{\text{NH}_3} = 2x = 0.25 \text{ atm}$

7. 
$$V_{\text{RMS}} = \sqrt{\frac{3RT}{M}} = \sqrt{\frac{3P}{\rho}} = \sqrt{\frac{3 \times 1.2 \times 10^5}{4}} = 300 \text{ m/s}$$

8.  $[(v_{\text{rms}})_X]_{546^\circ\text{C}} = [(v_{\text{mp}})_Y]_{273^\circ\text{C}}$
- $$\sqrt{\frac{3RT_X}{M_X}} = \sqrt{\frac{2RT_Y}{M_Y}} \quad \frac{3 \times 819}{9} = \frac{2 \times 546}{M_Y}$$
- $\therefore M_Y = 4 \text{ amu.}$

9. (C) Area under the curve  $\left(\frac{1}{N} \frac{dN}{dv}\right)$
- 
- $$= \int_0^x y dx = \int_0^N \left(\frac{1}{N} \frac{dN}{dV}\right) dV = \frac{1}{N} \int_0^N dN = 1.$$

11. (C,D)  
 If two gases have identical Maxwellian plots then their all the speeds will also be identical.

Hence  $\frac{T_A}{M_A} = \frac{T_B}{M_B}$ . Since all the speeds are proportional to  $\sqrt{\frac{T}{M}}$

for  $\text{SO}_2$  -  $M_1 = 64, T_1 = 600 \text{ K}$ ;  $\text{O}_2$  -  $M_2 = 32, T_2 = 300 \text{ K} \Rightarrow \frac{T_1}{M_1} = \frac{T_2}{M_2}$ .

## DPP No. # 33

1. (a) V.P. depends on temperature.
3. Pressure of air =  $750 - 100 = 650 \text{ mm of Hg}$   
 on compressing  $P_f = \text{Hg } 650 \times 3 \text{ mm of Hg}$   
 $= 1950 \text{ mm of Hg}$   
 so  $P_T = (1950 + 100) = 2050 \text{ mm of Hg}$
4.  $P_{\text{N}_2} + P_{\text{H}_2\text{O}(v)} = 1 \text{ atm}, \therefore P_{\text{H}_2\text{O}} = 0.3 \text{ atm}$

$$\therefore P_{N_2} = 0.7 \text{ atm}$$

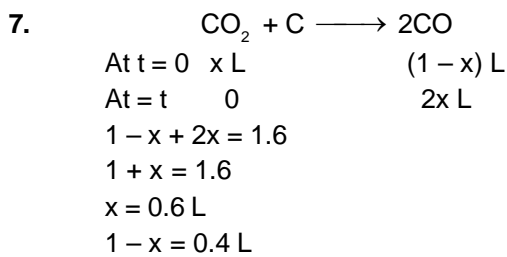
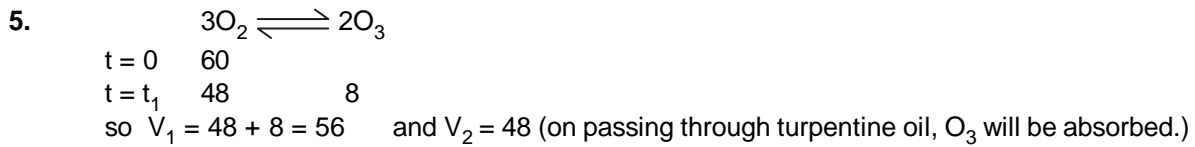
Now new pressure of  $N_2$  in another vessel of volume  $V/3$  at same  $T$  is given by :

$$P_{N_2} \times \frac{V_1}{3} = 0.7 \text{ atm} \times V_1$$

$$\therefore P_{N_2} = 2.1 \text{ atm}$$

Since aqueous tension remains constant, and thus total pressure in new vessel.

$$= P_{N_2} + P_{H_2O} = 2.1 + 0.3 = 2.4 \text{ atm.}$$



8. 896 mL.

### DPP No. # 34

- $T_4 < T_3 < T_2 < T_1$
- A real gas behaves ideally under conditions of low pressure and high temperature.
- Order of Vander waals constant  $CO_2 > CH_4 > N_2 > H_2$   
 $\therefore$  ease of liquification  $CO_2 > CH_4 > N_2 > H_2$
- \*  $Z$  for an ideal gas is equal one.
- Clearly, from the graph at 80 K  $Z = \frac{PV}{RT} = 1$  and at 60K,  $Z < 1$

7.  $Z = \frac{PV}{nRT} \Rightarrow n = \frac{PV}{ZRT}$

8. Translational energy =  $(3/2) kT$   
 =  $(3/2) kT = hcR_H ((1/1) - (1/4))$

$$= (3/2) T = 6.626 \times 10^{-34} \times 2.996 \times 10^{10} \times 109679 \times (3/4) \frac{6.02 \times 10^{23}}{8.315}$$

$$= 118331.1 \text{ K}$$

$$T = 118331.1 \times 2/3 = 80000 \text{ K.}$$

### DPP No. # 35

4. For very large value of molar volume ( $V_m$ )

$\frac{a}{V_m}$  and  $b$  can be neglected, so gas behaves as Ideal

$$\therefore PV_m = RT$$

5. At low pressure vander waal's equivalent for a real gas is given as

$$Z = 1 - \frac{a}{RTV}$$

intercept = 1

slop = -ve

$$7. \quad (i) \quad Z = \frac{PM}{dRT} = \frac{2 \times 16}{0.8 \times \frac{1}{12} \times 400} = 1.2$$

(ii) As  $Z > 1$ , so repulsive forces are dominating among gas molecules.

8. At Boyle's temperature, for low pressure regions,  $Z = 1$ . However, for high pressure regions,  $Z > 1$ .

### DPP No. # 36

4. Under low pressure region and below the boyle temperature,  $Z < 1$ .

5. Refer class notes.

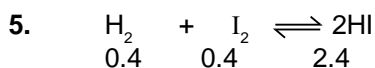
$$7.* \quad \text{at very high Pressure } Z = 1 + \frac{Pb}{RT}$$

$$Z > 1$$

for particular realgas above boyle temp  $Z > 1$ .

8.  $[A - r]$  ;  $[B - r, s]$  ;  $[C - q]$  ;  $[D - r]$ .

### DPP No. # 37



$$K = \frac{2.4 \times 2.4}{0.4 \times 0.4} = 36 \quad (\text{Since volume term is cancelled})$$

7. Mol. mass of HI = 1 + 127 = 128

64 g HI = 64 / 128 = 0.5 mole

$$[\text{HI}] = \frac{0.5}{2} \quad M = 0.25 \text{ M}$$

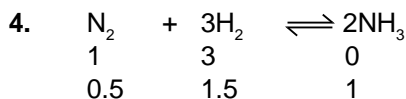
### DPP No. # 38

$$1. \quad K_p = K_c (RT)^{\Delta n}$$

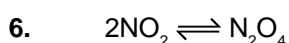
$$2K_c = K_c (RT)^{\Delta n}$$

$$2 = (RT)^1$$

$$T = \frac{2}{0.0821} = 24.36 \text{ K}$$



$$P_{\text{H}_2} = \frac{1.5}{3} P = P/2$$



$$K_c = \frac{[\text{N}_2\text{O}_4]}{[\text{NO}_2]^2} = \left( = \frac{\text{mol L}^{-1}}{(\text{mol L}^{-1})^2}, K_c \text{ has unit of } \text{L mol}^{-1} \right)$$

$$K_p = \frac{P_{N_2O_4}}{P_{NO_2}^2} \left( = \frac{\text{atm}}{\text{atm}^2}, K_p \text{ has unit of } \text{atm}^{-1} \right)$$

(Since mole fraction is itself unitless hence,  $K_x$  is also unitless)

7. (i) Molar concentrations :

$$[PCl_3] = \frac{\text{mol}}{L} = \frac{1}{2} = 0.5 \text{ mol L}^{-1}$$

$$[PCl_3] = \frac{2}{2} = 1.0 \text{ mol L}^{-1}$$

$$[Cl_2] = \frac{2}{2} = 1.0 \text{ mol L}^{-1}$$

(ii) Mole fractions :

Total moles at equilibrium = 1 + 2 + 2 = 5

$$\therefore X_{PCl_5} = \frac{n_{PCl_5}}{n_{\text{total}}} = \frac{1}{5} = 0.2$$

$$X_{PCl_3} = \frac{n_{PCl_3}}{n_{\text{total}}} = \frac{2}{5} = 0.4$$

$$X_{Cl_2} = \frac{n_{Cl_2}}{n_{\text{total}}} = \frac{2}{5} = 0.4$$

(iii) Equilibrium constants :

$$K_c = \frac{[PCl_3][Cl_2]}{[PCl_5]} = \frac{1 \times 1}{0.5} = 2 \text{ (mol L}^{-1}\text{)}^{-1} = 2 \text{ L mol}^{-1}$$

8.  $K_c = 4.0$ .

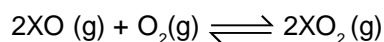
9.  $PCl_3 + Cl_2 \rightleftharpoons PCl_5$   
 $t = 0$      $n$          $n$          $0$   
 $t = \text{teq.}$   $n-y$      $n-y$      $y$

$$K_p = \frac{y}{(n-y)(n-y)} \left[ \frac{P}{2n-y} \right]^{-1}$$

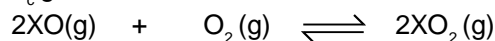
$$K_p = \frac{(2n-y)y}{(n-y)^2 P}$$

### DPP No. # 39

8. The equilibrium reaction is



since the unit of  $K_c$  given is lit/mole.



Initial conc.        1                    2                    0  
 Conc. at equilib.    $1-2x$              $2-x$                  $2x$

$$\therefore K_c = \frac{[XO_2]^2}{[XO]^2 [O_2]} = \frac{(2x)^2}{(1-2x)^2 (2-x)} = \frac{4x^2}{(1-2x)^2 (2-x)} = \frac{4x^2}{2}$$

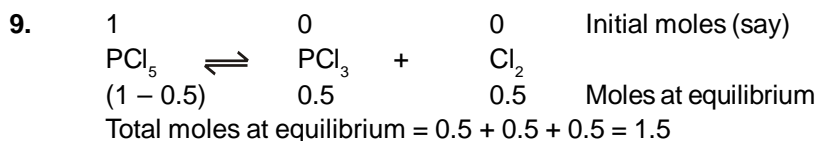
Since, the value of equilibrium constant is very small ( $1 \times 10^{-4}$ ), so  $2x$  can be ignored with respect to 1 and  $x$  can be ignored with respect to 2.

$$\therefore 1 \times 10^{-4} = \frac{4x^2}{2}$$

$$x = 7.07 \times 10^{-3}$$

we can see that the value of  $x$  is very small, so the assumption made was correct as it is within 1.4% of the actual value. Thus, the assumption made is correct and acceptable.

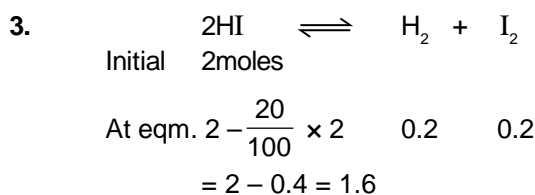
$$\begin{aligned} \therefore [XO] &= 1 - 0.01414 = 0.985 \text{ M} \\ [O_2] &= 2 - 0.00707 = 1.992 \text{ M} \\ [XO_2] &= 0.0141 \text{ M} \end{aligned}$$



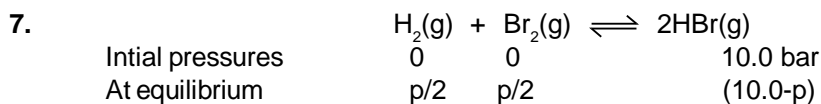
$$K_p = \frac{P_{PCl_3} \cdot P_{Cl_2}}{P_{PCl_5}} = \frac{\left(\frac{0.5}{1.5}p\right)\left(\frac{0.5}{1.5}p\right)}{\left(\frac{0.5}{1.5}p\right)} \quad (p = \text{total pressure})$$

or  $K_p = \frac{1}{3} \cdot p$  or  $p = 3K_p$ .

### DPP No. # 40



$$K = \frac{[H_2][I_2]}{[HI]^2} = \frac{0.2 \times 0.2}{(1.6)^2} = \frac{1}{64}$$



$$K_p = \frac{p_{HBr}^2}{p_{H_2} \times p_{Br_2}}$$

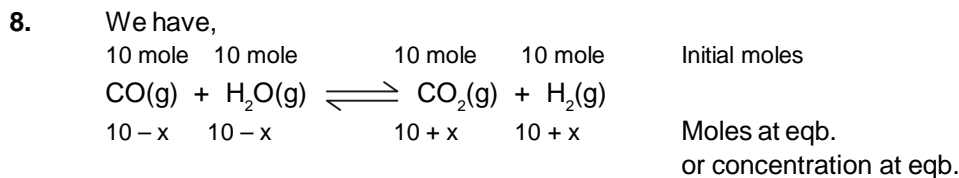
$$1.6 \times 10^5 = \frac{(10-p)^2}{(p/2)(p/2)}$$

Taking square root of both sides

$$4 \times 10^2 = \frac{10-p}{p/2}$$

$$200p = 10 - p; \quad p = \frac{10}{201} \text{ bar}$$

$$p_{H_2} = p/2 = \frac{1}{2} \left( \frac{10}{201} \right) \text{ bar} = 2.5 \times 10^{-2} \text{ bar}; \quad p_{Br_2} = p/2 = 2.5 \times 10^{-2} \text{ bar}; \quad p_{HBr} = 10 - p \approx 10 \text{ bar}.$$



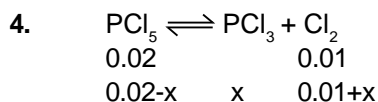
where x is the number of moles of each reactant changed to the products at equilibrium.

$$K = \frac{(10+x)^2}{(10-x)^2} = 9/4 \text{ (given)} \quad \text{or} \quad \frac{10+x}{10-x} = 3/2; \quad x = 2$$

$$\text{Mole percent of } H_2(g) \text{ at equilibrium} = \frac{10+x}{40} \times 100 = 30$$

### DPP No. # 41

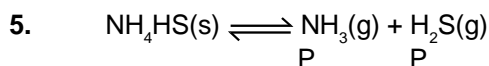
3. 0.2.



$$D = \frac{PM}{RT}$$

Calculate  $M_{\text{avg}}$ .

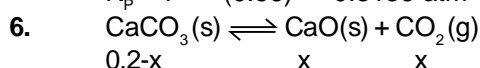
$$\frac{(0.02-x)208.5 + 137.5x + (0.01+x)71}{0.03+x} = M_{\text{avg}}$$



$$2P = 1.12$$

$$P = 0.56$$

$$K_p = P^2 = (0.56)^2 = 0.3136 \text{ atm}^2$$



$$K_p = P_{\text{CO}_2} = 1$$

$$x = \text{mole of CO}_2 = \frac{PV}{RT}$$

Remaining mass of  $\text{CaCO}_3 = (0.2 - x) 100 \text{ g}$ .

7. 
$$[\text{CaO}] = \frac{P_{\text{CaO(s)}}}{M_{\text{CaO(s)}}} = \frac{1.12}{56} \times 1000$$

- 9.\* Addition of solids have no effect on equilibrium and temperature favours endothermic direction while increasing pressure will shift equilibrium in backward direction as  $\Delta n_g$  is +ve.

### DPP No. # 42

2. 
$$K_p = (p_{\text{H}_2\text{O}})^4 = 2.56 \times 10^{-10} \text{ atm}^4$$
  

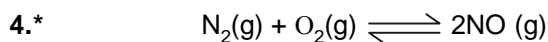
$$\therefore p_{\text{H}_2\text{O}} = 4 \times 10^{-3} \text{ atm} = 4 \times 10^{-3} \times 760 = 3.04 \text{ torr}$$

$$\text{Partial pressure of water vapour in air} = \frac{40}{100} \times 12.5 = 5$$

So, the amount of water vapour in air should decrease to decrease value of partial pressure of water vapour from 5 torr to the equilibrium value (3.04 torr).

so, mass of  $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$  will increase and mass of  $\text{CuSO}_4 \cdot \text{H}_2\text{O}$  will decrease.

3. (A) As reaction is endothermic therefore it will go in the forward direction hence moles of  $\text{PbO}$  will increase.  
 (B) With the increase or decrease of volume partial pressure of the gases will remain same.  
 (C) Due to the addition of inert gas at constant pressure reaction will proceed in the direction in which more number of gaseous moles are formed.



(A) For changing pressure volume has to be changed, though number of moles of  $\text{NO(g)}$  do not get changed but its concentration will get changed.

(B) Temperature change will change  $K_p$  and hence concentration.

(C) Volume change will change concentration, not the number of moles.

(D) Catalyst does not change equilibrium concentrations.

- 5.\* Number of moles will remain unchanged but due to decreased volume pressure will get increased and also the concentrations.

6. Slope =  $-\tan 30^\circ = \frac{-1}{\sqrt{3}} = \frac{-\Delta H^\circ}{R}$

$\therefore \Delta H^\circ = \frac{R}{\sqrt{3}}$

7. As  $T \rightarrow \infty$ ,  $K = A$

$\therefore \ln A = \ln K = 46.06$

$\therefore 2.303 \log_{10} A = 46.06$

$\therefore A = 10^{20}$

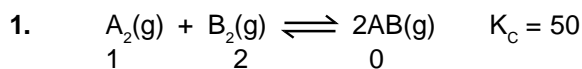
8.  $\Delta H^\circ > 0$   $\therefore$  Endothermic reaction

Y-intercept = +ve  $\therefore \Delta S^\circ > 0$

for endothermic reaction, as  $T \uparrow$ ,  $K \uparrow$ .

The value of equilibrium constant K is unaffected by pressure changes.

### DPP No. # 43



1-x	2-x	2x
3	3	3

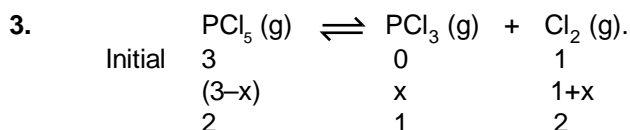
$$50 = \frac{\frac{2x}{3} \cdot \frac{2x}{3}}{\frac{1-x}{3} \cdot \frac{2-x}{3}} = \frac{4x^2}{(1-x)(2-x)} = \frac{4x^2}{2-3x+x^2} \Rightarrow 100 - 150x + 50x^2 = 4x^2$$

$\therefore$  no. of mol of AB =  $\frac{2x}{3} = 1.868$ .

$\therefore$  AB density  $k = \frac{2x}{3} = 1.868$

2. (i) From the graph  $0.3 \times n = 0.6$   
 $n = 2$

(ii)  $K = (0.6)^2 / 0.3 = 1.2 \text{ mol / L}$



Initial total moles =  $(3+1) = 4$ .

Now from Ideal gas equation

$PV = nRT = P \times 100 = 4 \times 0.082 \times 500$

$P = 0.082 \times 20 = 1.64 \text{ atm.}$

At equilibrium Total mole =  $3 - x + x + 1 + x = (4 + x)$

$PV = nRT$ .

$2.05 \times 100 = (4+x) \times 0.082 \times 500$ .

$2.05 = (4+x) \times 0.41$ .

$5 = 4 + x$ .

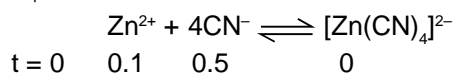
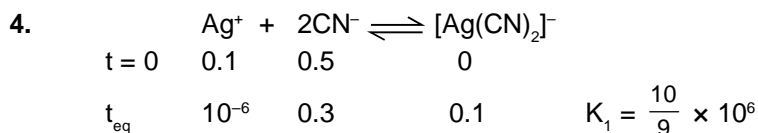
$x = 1$ .

$\alpha = \frac{\text{No. of mole dissociated}}{\text{Initially total mole taken}} = \frac{1}{3} = 0.33$ .

$P_{PCl_5} = \frac{2}{5} \times 2.05$  ;  $P_{PCl_3} = \frac{1}{5} \times 2.05$

$P_{Cl_2} = \frac{2}{5} \times 2.05$

$K_p = \frac{\left(\frac{1}{5} \times 2.05\right) \left(\frac{2}{5} \times 2.05\right)}{\left(\frac{2}{5} \times 2.05\right)} = [0.41]$



eq.	10 <sup>-12</sup>	0.1	0.1	$K_2 = \frac{0.1}{(0.1)^4 \times 10^{-12}} = 10^{15}$
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Subtracting two times I<sup>st</sup> reaction from II<sup>nd</sup> reaction, we will get the required reaction, so

$$K_{\text{eq}} = \frac{10^{15}}{\left(\frac{10}{9}\right)^2 \times 10^{12}} = \frac{10^3 \times 81}{100} = 810 \quad \text{Ans. 810}$$

- 5.\* When some amount of HCl is added to equilibrium, the first eq will shift in backward direction leading to decrease in amount of O<sub>2</sub>. Then, the second eq. will shift in backward direction to increase the amount of O<sub>2</sub>. Thus, amount of N<sub>2</sub> gas will increase.

### DPP No. # 44

4. (i) Molecules move faster for which  $\frac{T}{M}$  greater obviously H<sub>2</sub> molecule move faster.
5. State function : a, b, c, d, g, h, j ; Path function : e, f, i, k
6. Intensive : a, c, d, f, g, h, i, k ; Extensive : b, e, j, l
7. Open system : b, f, g, i, j ; Closed system : a, c, h ; Isolated system : d, e
8. Q = 7.5 KJ  
 $\Delta U = -12$  KJ  
 $\Delta U = Q + W$   
 $W = -12 - 7.5 = -19.5$  KJ. Ans.  
 Now W = 0,  
 $\therefore \Delta U = Q \quad \therefore Q = \Delta U = -12$  KJ Ans.

### DPP No. # 45

5.  $\Delta U_{ab} = Q_{abc} + W_{abc}$   
 or  $\Delta U_{ab} = 100 - 40 = 60$  J  
 $\Delta U_{ab} = Q_{aeb} + W_{aeb}$   
 or  $60 = Q_{aeb} - 20$   
 or  $Q_{aeb} = 80$  J **Ans.**
- $\Delta U_{ba} = -60$  J  
 $W_{bda} = 30$  J  
 $\Delta U_{ba} = Q_{bda} + W_{bda}$   
 or  $Q_{bda} = \Delta U_{ba} - W_{bda}$   
 or  $Q_{bda} = -60 - 30 = -90$  J **Ans.**

Since Q<sub>bda</sub> is (-)ve  $\therefore$  Heat is liberated from the system.

6. 4275 J.
7. 6.66 min. (400 sec)
8. Since  $\Delta E = q + w$   
 $= 80 - 30 = 50$   
 So for ADB  
 $\Delta E = q + w$



$$50 = q - 10$$

$$q = 60 \text{ J}$$

9. For B to A,

$$\Delta E = -50 \text{ J}$$

$$w = +20 \text{ J}$$

$$q = -50 - 20 = -70$$

heat is liberate.

10. In ADB process, DB process is isochoric so  $w_{DB} = 0$

$$\text{So, } \Delta E_{AD} = q_{AD} + w_{AD}$$

$$-40 = q_{AD} + (-10)$$

$$q_{AD} = -30 \text{ J}$$

$$\text{Now, } q_{AB} = q_{AD} + q_{DB}$$

$$60 = -30 + q_{DB}$$

$$q_{DB} = 90 \text{ J}$$

### DPP No. # 46

1.  $w = P_{\text{ext}} \Delta V$

$$w = -1.2 \times 32 = -38.4 \text{ lt atm.}$$

$$= -38.4 \times 100 \text{ J} = -3840 \text{ J} = -3.84 \text{ kJ}$$

$$\Delta E = q + w$$

$$\text{so, } q = \Delta E - w = -51 + 3.84 = -47.16.$$

6.  $W = 240 \text{ L atm.}$

7.  $\Delta U = \Delta H = 0 \quad Q = -W$

$$W = -2.303 nRT \log \frac{V_2}{V_1} \quad \Rightarrow \quad W = -2.3 \times \frac{20}{40} \times 8.3 \times 300 \log \frac{10}{5} = -859.05 \text{ J.}$$

8. (a)  $W = -nRT \ln \frac{V_2}{V_1}$

$$W = -P_1 V_1 \ln \frac{V_2}{V_1} = -14 \times 0.03 \ln \frac{0.06}{0.03} \text{ bar m}^3 = -14 \times 0.7 \times 0.03 = -0.294 \text{ bar m}^3 \text{ Ans.}$$

(b)  $P_1 V_1 = P_2 V_2$

$$\therefore P_2 = \frac{P_1 V_1}{V_2} = \frac{14 \times 0.03}{0.06} = 7 \text{ bar}$$

$$\therefore W = -P_{\text{ext}} (V_2 - V_1) = -7 (0.06 - 0.03) = -7 \times 0.03 = -0.21 \text{ bar m}^3.$$

$$\text{Efficiency} = \frac{0.21}{0.294} = 71.43\% \text{ Ans.}$$

9. (a) F (b) T (c) F (d) T (e) T

### DPP No. # 47

1. The product PV is increasing so temperature will keep or increasing in the process, hence

$$\Delta H = \Delta E + \Delta(PV) \text{ will increase constantly.}$$

2. From graph we know that  $V_B > V_A$ , so expansion has taken place so w will be with -ve sign and  $\Delta H$  will be +ve as both  $\Delta E$  and  $\Delta(PV)$  have increased.

3. At A and D the temperatures of the gas will be equal, so

$$\Delta E = 0, \quad \Delta H = 0$$

$$\text{Now } w = W_{AB} + W_{BC} + W_{CD} = -P_0 V_0 - 2P_0 V_0 \ln 2 + P_0 V_0 = -2P_0 V_0 \ln 2$$

$$\text{and } q = -w = 2P_0 V_0 \ln 2$$

5. Since liquid is expanding against external pressure  $P_0$  hence work done

$$w = -P_0 (4V_0 - V_0) = -3P_0 V_0$$

$$\Delta U = w = -3P_0 V_0$$

$$\Rightarrow \Delta H = \Delta U + P_2 V_2 - P_1 V_1 = -3P_0 V_0 + 4P_0 V_0 - 2P_0 V_0.$$

7.  $\gamma$  for  $O_2 = 1.44$   $\gamma$  for He = 1.66.

8. Since,  $\Delta H$  is a state function, and the final state attained by the gas is same as its initial state, so value of  $\Delta H = 0$ .

9.  $q = q_{AB} + q_{BC} + q_{CD} + q_{DA}$   
 $= -1R \times 300 \ln 2 + 1 \times \frac{5R}{2} \times (400 - 300) + 1R \times 400 \ln 2 + 1 \times \frac{5R}{2} \times (300 - 400)$   
 $(\because q_{AB} = -W_{AB} = -1R \times 300 \ln 2$  since process is reversible isothermal for which  $\Delta U = 0$ ).  
 $(\because q_{BC} = \Delta H_{BC} = 1 \times \frac{5R}{2} \times (400 - 300)$  since process is reversible isobaric).  
 $(\because q_{CD} = -W_{CD} = 1R \times 300 \ln 2$  since process is reversible isothermal for which  $\Delta U = 0$ ).  
 $(\because q_{DA} = \Delta H_{AB} = 1 \times \frac{5R}{2} \times (300 - 400)$  since process is reversible isobaric).  
 So,  $q = 100 R \ln 2$ .

10. Since, for a cyclic process,  $\Delta U = 0$ .  
 So,  $W = -q = -100 R \ln 2$ .

### DPP No. # 48

1.  $TV^{\gamma-1} = \text{constant}$

$$\gamma = \frac{5}{3} \quad \therefore \quad \gamma - 1 = \frac{2}{3}$$

$$\therefore \quad 300 \times (8)^{2/3} = 250 \times (V_2)^{2/3} \quad \Rightarrow \quad (V_2)^{2/3} = 4.8$$

$$\Rightarrow \quad V_2 = (4.8)^{3/2} \cong 4.8 \times 2.2 = 10.5 \text{ L}$$

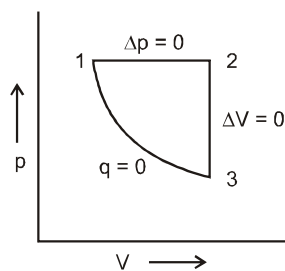
8.  $\gamma_{\text{mix}} = \frac{n_A C_{PA} + n_B C_{PB}}{n_A C_{VA} + n_B C_{VB}} = \frac{2(4R) + 4(5R/2)}{2(3R) + 4(3R/2)} = \frac{18R}{12R} = \frac{3}{2}$

$$T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1} \quad (\gamma = \gamma_{\text{mix}} = 1.5)$$

$$\therefore \quad T_2 = 320 \left( \frac{2}{8} \right)^{1.5-1} = 320 \times \frac{1}{2} = 160 \text{ K}$$

$$\therefore \quad W = \frac{nR}{\gamma-1} (T_2 - T_1) = \frac{6R}{1.5-1} (160 - 320) = -1920 R = 1920 \times 2 = -3840 \text{ calories.}$$

9. The process can be described on a p-V diagram as



At 1 : $p = 10 \text{ atm}$	$T = 400 \text{ K}$	$V = V_1$
At 2 : $p = 10 \text{ atm}$	$T = 800 \text{ K}$	$V = V_2 = 2V_1$
At 3 : $p = ?$	$T = T_3$	$V = V_3 = V_2 = 2V_1$

Therefore,

$$W_{12} = -p\Delta V = -nRT = -400 R$$

$$W_{23} = 0$$

$[\because \Delta V = 0]$

Between 3 and 1 ;  $TV^{\gamma-1} = \text{constant}$

$$T_3 (2V_1)^{\gamma-1} = 400(V_1)^{\gamma-1}$$

$$\Rightarrow T_3 = 400 \left(\frac{1}{2}\right)^{2/3} = 252 \text{ K}$$

$$\Rightarrow W_{31} = \Delta E_{31} = nC_V(T_1 - T_3) = \frac{3}{2} R(400 - 252) = 222 \text{ R}$$

$$\Rightarrow W_{12-31} = W_{12} + W_{23} + W_{31} = -178 \text{ R}$$

10.  $W = -\int PdV$

$$= -\int \frac{K}{V^n} dV = -\frac{K}{1-n} \left[ V^{-n+1} \right]_{V_1}^{V_2} = \frac{K}{n-1} [V_2^{1-n} - V_1^{1-n}]$$

$$= \frac{P_1 V_1^n}{n-1} [V_2^{1-n} - V_1^{1-n}] = \frac{P_1 V_1^{n+1-n}}{n-1} \left[ \left(\frac{V_2}{V_1}\right)^{1-n} - 1 \right]$$

### DPP No. # 49

1. Standard molar enthalpy of formation ( $\Delta H_f^\circ$ ) of element in their stable state of aggregation is zero.

$$\therefore \Delta H_f^\circ (\text{O}_2, \text{g}) = 0$$

4. Some of the heat is used to vaporise the  $\text{H}_2\text{O} (\ell)$

$$\therefore x_1 > x_2$$

5.  $\text{CS}_2(\ell) + 3\text{O}_2(\text{g}) \longrightarrow \text{CO}_2(\text{g}) + 2\text{SO}_2(\text{g}) ; \quad \Delta H_{\text{rxn}}^\circ = 5 \times -215 = -1075 \text{ kJ}$

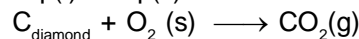
$$\Delta H_{\text{rxn}}^\circ = \Delta H_f^\circ (\text{CO}_2) + 2 \times \Delta H_f^\circ (\text{SO}_2) - \Delta H_f^\circ (\text{CS}_2)$$

$$\Delta H_{\text{rxn}}^\circ = (-393.5 - 2 \times 296.8) - (-1075)$$

$$\Delta H_{\text{rxn}}^\circ = 87.9$$

6. Refer Class notes.

8. Eq (i) + Eq (ii)



$$\Delta H = \Delta H_1 + \Delta H_2$$

### DPP No. # 50

2. Since it is neutralisation of a weak acid with strong base.

3. enthalpy of dissociation =  $(13.7 - 3) \text{ KCal} = 10.7 \text{ KCal}$

6.  $n_{\text{CH}_4} = \frac{280}{22.4}$

$$\therefore \Delta H_{\text{obtained}} = \frac{240 \times 280}{22.4} \text{ KCal}$$

$$\therefore m = \frac{240 \times 280}{22.4 \times 2 \times 1 \times 180} \text{ kg} = 8.33 \text{ kg.}$$

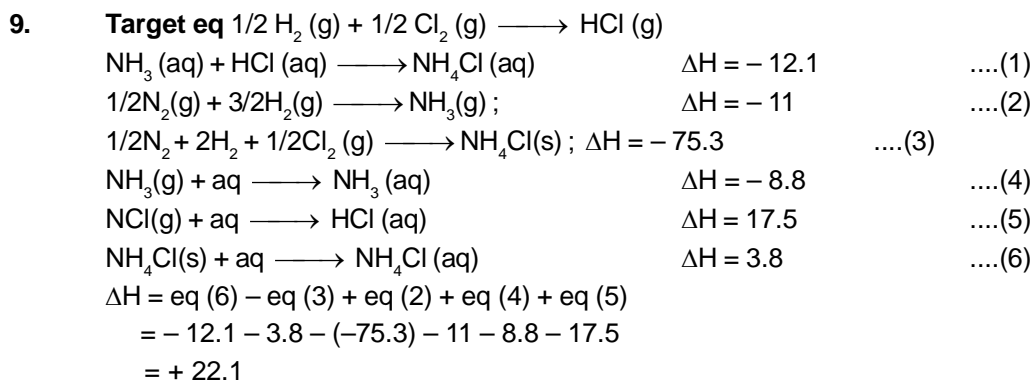
7. Heat generated =  $C_T \Delta T = 1260 \times 0.667 \text{ cal.}$

$$\therefore n_{\text{CH}_4} = \frac{1260 \times 0.667}{210 \times 10^3}$$

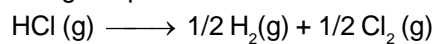
$$n_{\text{total}} = \frac{PV}{RT} = 4 \times 10^{-2} \quad \therefore \text{mol\%} = \frac{4 \times 10^{-3}}{4 \times 10^{-2}} \times 100\% = 10\% \text{ Ans.}$$

8.  $\Delta H_2 - 24 = -0.024 \times (523 - 473) \text{ Cal/g.}$

$$\therefore \Delta H_2 = 22.8 \text{ Cal/g.}$$



from this we get equation



$\therefore \Delta\text{H}$  of target eq =  $-\Delta\text{H} = -22.1 \text{ Kcal Ans.}$